

**IN THE SPECIFICATION:**

Please replace the paragraph beginning on page 1, line 1 with the following amended paragraph:

The invention relates to the moving-bed processes such as gasoline reforming (reforming according to English terminology) for the improvement of the octane number of petroleum fractions that are located in the range of gasolines, i.e., at the starting point between 70°C and 110°C, and at the end boiling point between 150°C and 180°C. More generally, the invention relates to any process that uses a series of moving-bed reactors such as are found in the ~~spraying process (aromatizing according to English terminology)~~ aromatizing process or the process for dehydrogenating normal paraffins. The following description refers to the reforming process with continuous regeneration that will be designated by the name of regenerative reforming. The process for reforming gasolines started in the 1950s and has since known important technological developments that are often linked to the appearance of new generations of catalysts according to three successive stages. The appearance of catalyst was based on platinum on alumina in the 1950s. The units worked at pressures on the order of 5 MPa, and the catalyst was regenerated about every 6 months. Toward the end of the 1960s, the bimetallic catalysts that would allow the operating pressure to be lowered to around approximately 3 MPa appeared. Finally, at the beginning of the 1970s, the appearance of the continuous regeneration of catalyst made it possible to reach operating pressures only on the order of 1 MPa.

Please replace the paragraph beginning on page 3, line 3 with the following amended paragraph:

In the two cases, the effluents that are obtained from a reactor are heated in a furnace before being introduced at the top of the next reactor since, overall, the reactions that are involved are endothermic and the reactors are operated at the same starting temperature. In the technology with vertical stacking of the reactors, the catalyst flows by gravity from one reactor to the next, then it is picked up by a lift line (~~lift according to English terminology~~) or a pneumatic transport line at the outlet of the last reactor to be introduced at the top of the regenerator in

which it also flows by gravity. At the bottom of the regenerator, it is picked up by a second lift line to be introduced at the top of the first reactor.

Please replace the subheading beginning on page 5, line 1 with the following amended subheading:

Summary Brief Description of the Figures: